## Supporting information

## Utilization of activated carbon for the adsorption of methylene blue from waste coffee husk

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Intraparticle diffusion

Models Equation

Pseudo-first order  $q_t = q_e(1 - e^{-(k_1 \times t)})$ Pseudo-second order  $q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t}$ Elovich  $q_t = \frac{1}{\beta} ln(\alpha \beta t + 1)$ Bangham  $q_t = k_b t^{\alpha_b}$ 

Table S1: Adsorption kinetic models.

In which,  $q_t$  (mg  $g^{-1}$ ) is the amount of adsorbent over time t (min);  $k_1$  (min<sup>-1</sup>) is the constant rate of Pseudo-first order;  $k_b$  is the constant rate of Bangham;  $K_1$  (mg  $g^{-1}$  min<sup>-1</sup>) is the constant rate;  $\alpha$  (mg  $g^{-1}$  min<sup>-1</sup>) is the initial adsorption rate;  $\beta$  (g mg<sup>-1</sup>) is the desorption constant;  $\alpha_b$  (< 1) represents the adsorption intensity; C is a constant related to the thickness of the liquid film surrounding the adsorbent.

 $q_t = K_I t^{0,5} + C$ 

Table S2: Adsorption isotherm models

| Models            | Equation  |
|-------------------|---|
| Freundlich        | $q_e = K_F C_e^{1/n}$                                   |
| Temkin            | $q_e = b_T \ln A C_e$                                   |
| Redlich-Petterson | $q_e = \frac{K_{RP} C_e}{1 + \alpha C_e^{\beta}}$       |
| Sips              | $q_e = \frac{Q_m (K_S C_e)^{1/n}}{1 + (K_S C_e)^{1/n}}$ |

In which,  $K_F$  ((mg.g<sup>-1</sup>)(L.mg<sup>-1</sup>)<sup>1/n</sup>) is the Freundlich isotherm constant,  $C_e$  (mg.L<sup>-1</sup>) is the dye concentration at equilibrium, n is a parameter related to the surface heterogeneity;  $b_T$  is related to the thermal state of adsorption, A (L.mg<sup>-1</sup>) is the Temkin constant;  $K_{RP}$  (L.g<sup>-1</sup>) and  $\alpha$  (mg<sup>-1</sup>) are the constants of Redlich-Petterson,  $\beta$  is an exponent between 0 and 1 that represents the heterogeneity of the adsorbent;  $Q_m$  (mg.g<sup>-1</sup>) is the maximum adsorption

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capacity of the Sips isotherm,  $K_s$  (L.mg<sup>-1</sup>) is the Sips constant and n is the index of heterogeneity; for a homogeneous material n=1.

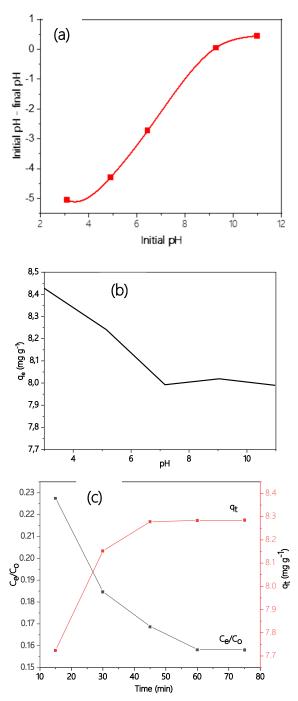


Figure S1:  $pH_{pzc}$  of AC (a), effect of pH on MB removal by AC after t = 60 min (b), and effect of contact time on MB adsorption capacity onto AC (c) ( $C_0 = 10 \text{ mg L}^{-1}$ , m = 0.05 g, V = 50 mL, T = 298 K).

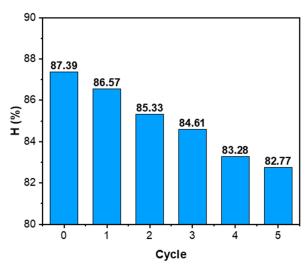


Figure S2: The reusability of AC as adsorbent for the removal of MB dye.